

Florida International University
Department of Civil and Environmental Engineering

CWR 3201 Fluid Mechanics

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Homework Assignment 4 Solutions

Mechanics of Fluids (Fifth edition), by M.C. Potter, D.C. Wiggert and B.H. Ramadan.

1. 4.35 (same number in *Fourth edition*)

Continuity Equation: $A_1 V_1 = A_2 V_2$

$$\pi(0.025^2) \left(\frac{10m}{s} \right) = (2\pi * 0.6 * \overset{0.003m}{\cancel{0.03}}) V_2$$

$$V_2 = \overset{1.736 \text{ m/s}}{\cancel{0.1736 \text{ m/s}}}$$

Mass flux: $\dot{m} = \rho AV = 1000 * \pi * 0.025^2 * \left(\frac{10m}{s} \right) = 19.63 \text{ kg/s}$

Flow Rate: $Q = AV = (2\pi * 0.6 * 0.03) * \overset{1.736}{\cancel{0.1736}} \frac{m}{s} = 0.0196 \frac{m^3}{s}$

2. 4.52 (same number in *Fourth edition*)

Maximum velocity is at the center of the tube in section 1: $V_{max} = 10(4 - 0^2) = 40 \text{ m/s}$

Average velocity at section 1: $\bar{V}_1 = \frac{V_{max}}{2} = 20 \text{ m/s}$

Conservation of mass: $\dot{m}_{in} = \dot{m}_2 + \dot{m}_3$

$$1000 * \pi * 0.02^2 * 20 \frac{m}{s} = 10 \frac{kg}{s} + 1000 * \pi * 0.02^2 * \bar{V}_3$$

$$\bar{V}_3 = 12.04 \text{ m/s}$$

3. 4.79 (same number in *Fourth edition*)

a) Across nozzle, continuity equation: $\pi * 0.07^2 * V_1 = \pi * 0.025^2 * V_2$

$$V_2 = 7.84 V_1$$

Bernoulli: $\frac{V_2^2}{2g} + \frac{p_2}{\gamma} = \frac{V_1^2}{2g} + \frac{p_1}{\gamma}$ $p_1 = 9810 \frac{7.84^2 - 1}{2 * 9.81} V_1^2$

For contraction: $\pi * 0.07^2 * V_1 = \pi * 0.05^2 * V_3$

$$V_3 = 1.96 V_1$$

Bernoulli: $\frac{V_3^2}{2g} + \frac{p_3}{\gamma} = \frac{V_1^2}{2g} + \frac{p_1}{\gamma}$

Manometer: $\gamma * 0.15 + p_1 = 13.6\gamma * 0.15 + p_3$ $\frac{p_1}{\gamma} = 12.6 * 0.15 + \frac{p_3}{\gamma}$

Sub all known values into Bernoulli: $\frac{V_3^2}{2g} + \frac{p_3}{\gamma} = \frac{V_1^2}{2g} + \frac{p_1}{\gamma}$ $\frac{V_1^2}{2g} + 12.6 * 0.15 = \frac{V_3^2}{2g} =$

$$1.96^2 \frac{V_1^2}{2g}$$

$$V_1 = 3.612 \text{ m/s}$$

$$p_1 = 394 \text{ kPa}$$

Reservoir surface to section 1: $\frac{V_0^2}{2g} + \frac{p_0}{\gamma} + z_0 = \frac{V_1^2}{2g} + \frac{p_1}{\gamma} + z_1$

$$H = \frac{V_1^2}{2g} + \frac{p_1}{\gamma} = 40.8 \text{ m}$$

b) Follows same method as part a.

4. 4.82 (same number in *Fourth edition*)

$$\frac{V_0^2}{2g} + \frac{p_0}{\gamma} + z_0 = \frac{V_1^2}{2g} + \frac{p_1}{\gamma} + z_1$$

$$\frac{80000 \text{ Pa}}{9810} + 4 = \frac{V_1^2}{2 * 9.81}$$

$$V_1 = 15.44 \text{ m/s}$$

$$Q = A_1 V_1 = \pi * 0.025^2 * 19.04 = 0.0303 \text{ m}^3/\text{s}$$

Part b and c only have different diameters for the flow rate equation.

5. 3.54 (same number in *Fourth edition*)

Using Bernoulli's Equation: $\frac{v^2}{2} = \frac{p}{\rho}$, where the density of air at 3000 ft is 0.0021 slugs/ft³

$$v = \sqrt{\frac{2p}{\rho}} = \sqrt{\frac{2(0.3 \text{ psi}) * \frac{144 \text{ in}^2}{1 \text{ ft}^2}}{0.0021 \text{ slugs/ft}^3}} = 203 \text{ ft/sec}$$

Part b and c are the same steps but with different pressures.

6. 3.68 (same number in *Fourth edition*)

Bernoulli: $\frac{V_2^2}{2g} + \frac{p_2}{\gamma} = \frac{V_1^2}{2g} + \frac{p_1}{\gamma}$, where the pressure at point 2 is the open end of the manometer so p_2 is equal to 0.

$$\text{Manometer: } p_1 + \gamma z + \gamma_{Hg} H - \gamma H - \gamma z = \frac{V_2^2}{2g} \gamma + p_2$$

$$\text{Substitute Bernoulli into the manometer equation: } p_1 + \gamma_{Hg} H - \gamma H = \frac{V_1^2}{2g} \gamma + p_1$$

$$H=0.01 \text{ m: } \frac{V_1^2 * 9800}{2 * 9.81} = (13.6)(9800) - (1)(9800) * 0.01$$

$$V_1 = 1.572 \text{ m/s}$$

$$\text{Plugging into Bernoulli: } p_1 = \frac{V_2^2 - V_1^2}{2g} \gamma = \frac{20^2 - 1.572^2}{2 * 9.81} * 9800 = 198562 \text{ Pa}$$

Other parts follow same solution

7. 13.9 (same number in *Fourth edition*)

$$\text{a. Manometer: } p_1 + \gamma_w h = p_2 + \gamma_w * SG_{mmHg} * h = p_1 + (9810)(0.12) = p_2 + 13.6(9810)(0.12)$$

$$p_1 - p_2 = 14832.7 \text{ Pa}$$

$$\frac{D_0}{D} = \frac{6}{12} = 0.5$$

$$\text{Head loss } h_1 - h_2 = \frac{p_1 - p_2}{\gamma_w} = \frac{14832.7 \text{ Pa}}{9810} = 1.51 \text{ m}$$

Try $Re = 10^5 \rightarrow K \approx 1.0$ (from graph 13.10)

$$Q = KA\sqrt{2g(h_1 - h_2)} = (1.0)(\pi/4 * 0.06^2)\sqrt{2(9.81)(1.51)} = 0.0154 \frac{\text{m}^3}{\text{s}}$$

Check: $V = \frac{Q}{A} = 5.45 \text{ m/s}$
1.362 m/s

$$Re = \frac{vD}{\nu} = \frac{(5.45)(0.12)}{0.658 * 10^{-6}} = 993920$$

2.47 * 10^5

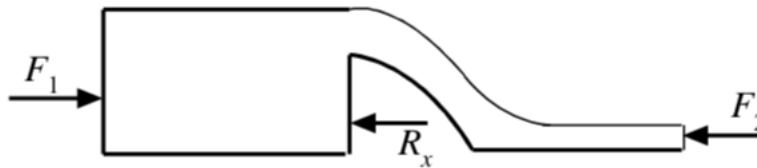
~~K=1.01 OK~~

Recalculate Q based on K=1.12, Q=0.0172 m/s. Another iteration will show that this guess is correct

b. Follows same procedure as part A except using curve for orifice on 13.10

graph: $Q = 0.0096 \frac{\text{m}^3}{\text{s}}$

8. 4.123 (same number in *Fourth edition*)



Continuity: $0.7V_1 = 0.1V_2 \quad V_2 = 7V_1$

Bernoulli (Energy): $\frac{V_1^2}{2g} + \frac{p_1}{\gamma} + h_1 = \frac{V_2^2}{2g} + \frac{p_2}{\gamma} + h_2$

$$\frac{V_1^2}{2(9.81)} + 0.7 = \frac{(7V_1)^2}{2(9.81)} + 0.1$$

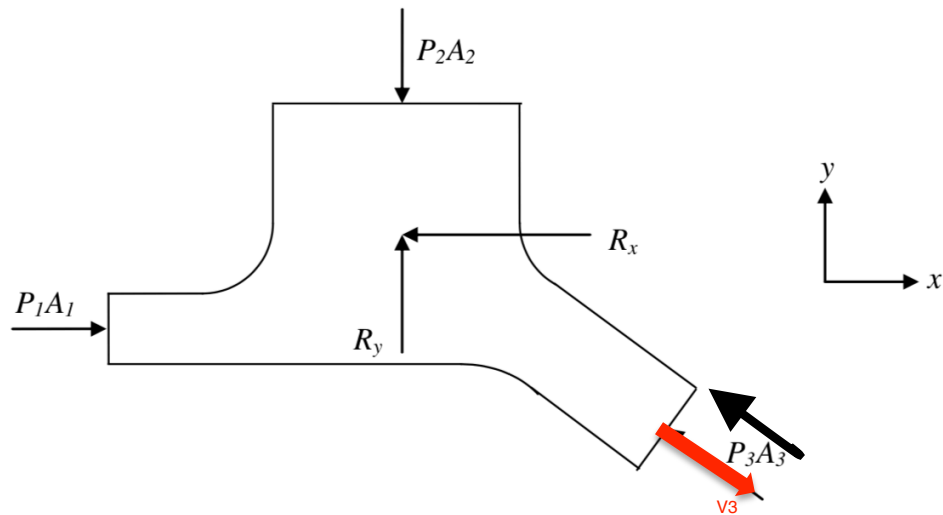
$$V_1 = 0.495, V_2 = 3.467 \text{ m/s}$$

Momentum: $F_1 - F_2 - R_x = \dot{m}(V_{out} - V_{in}) \rightarrow 9810 * \frac{0.7}{2} (0.7 * 1.5) - 9810 *$

$$\frac{0.1}{2} (0.1 * 1.5) - R_x = 1000(0.7 * 1.5)(0.495)(3.467 - 0.495)$$

$$R_x = 1987 \text{ N}$$

9. 4.131 (same number in *Fourth edition*)



$$\text{Mass flow rates: } \dot{m}_1 = \rho V_1 A_1 = 1000 * (15) * \left(\frac{\pi}{4} * 0.2^2\right) = 471 \text{ kg/s}$$

$$\dot{m}_2 = \rho V_2 A_2 = 1000 * (5) * \left(\frac{\pi}{4} * 0.45^2\right) = 795 \text{ kg/s}$$

$$\dot{m}_3 = \dot{m}_1 + \dot{m}_2 = 1266 \text{ kg/s}$$

$$V_3 = \frac{\dot{m}_3}{\rho A_3} = 25.8 \text{ m/s}$$

Conservation of momentum in the x: $p_1 A_1 - p_3 A_3 \cos 40 - R_x = \dot{m}_3 V_3 \cos 40 - \dot{m}_1 V_1$

Solving for $R_x = -16495 \text{ N}$

Conservation of momentum in y: $R_y - p_2 A_2 + p_3 A_3 \sin 40 = \dot{m}_3 (-V_3 \sin 40) - \dot{m}_2 (-V_2)$

Solving for $R_y = -17612.92 \text{ N}$

10. 4.164 (same number in *Fourth edition*)

Velocity through the nozzle: $V_e = \frac{\dot{m}}{\rho A} = \frac{4 \text{ kg/s}}{1000 * 4 * \left[\frac{\pi}{4} * 0.008^2\right]} = 19.89 \text{ m/s}$

$$\begin{aligned} M_{Inertia} \int_{c.v} r \times (2\Omega \times V) \rho d \text{Volume} &= 4 \int_0^{0.3} r \hat{i} \times (-2\Omega \hat{k} \times V \hat{i}) \rho A dr \\ &= 8\rho AV\Omega \hat{k} \int_0^{0.3} r dr = -0.36\rho AV\Omega \hat{k} \end{aligned}$$

Sum of the moments must equal zero

For steady flow: $\sum M - (M_I)_Z = \int_{c.s.} (r \times V) V \cdot \hat{n} \rho A d = 0.3 \hat{i} \times (0.707 V_e \hat{j} + 0.707 V_e \hat{k}) V_e \rho A$

Solving for $-(M_I)_Z = 0.36\rho AV\Omega = 4 * (0.3 * 0.707V_e^2 A_e\rho$

Continuity: $AV = V_e A_e$

$$0.36\Omega = 4 * (0.707 * 0.3)(19.89)$$

$$\Omega = 46.9 \text{ rad/s}$$