Contaminant Transport Equations

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Transport

Advection

- The process by which solutes are transported by the bulk of motion of the flowing ground water.
- Nonreactive solutes are carried at an average rate equal to the average linear velocity of the water.

Hydrodynamic Dispersion

- Tendency of the solute to spread out from the advective pathway
- Two processes

Diffusion (molecular and turbulent) Dispersion (velocity differences in space)

Diffusion

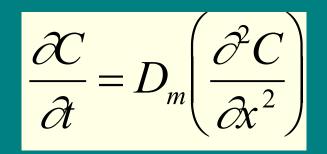
- Ions (molecular constituents) in solution move under the influence of kinetic activity in direction of their concentration gradients.
- Occurs in the absence of any bulk hydraulic movement
- Diffusive flux is proportional to concentration gradient, per *Fick's First Law (M L⁻²T⁻¹).*

$$F = -D_m \left(\frac{dc}{dx}\right)$$

• Where $D_m = diffusion$ coefficient (typically 1 x 10⁻⁵ to 2 x 10⁻⁵ cm^{2/s} for major ions in ground water)

Diffusion (continued)

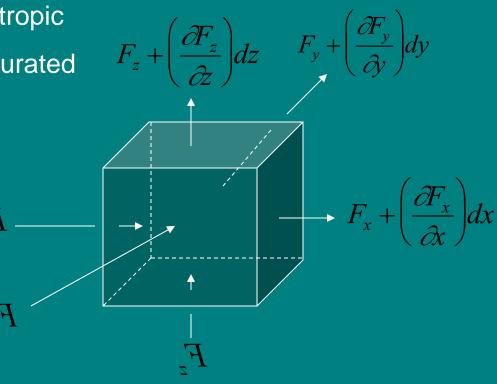
 Fick's Second Law - derived from Fick's First Law and the Continuity Equation - called "Diffusion Equation"



The Advection-Dispersion Equation Derivation (F is transport flux)

Assumptions:

- 1) Porous medium is homogenous
- 2) Porous medium is isotropic
- 3) Porous medium is saturated
- 4) Flow is steady-state
- 5) Darcy's Law applies



Advection Dispersion Equation

In the x-direction:

Transport by advection = $\overline{v}_x nCdA$ units $\frac{NI}{T}$

Transport by dispersion =
$$nD_x \left(\frac{\partial C}{\partial x}\right) dA$$
 units $\frac{M}{T}$

Where:

- \overline{v} = average linear velocity
- n = porosity (constant for unit of volume)
- C = concentration of solute

dA = elemental cross-sectional area of cubic element

 $D_x = \alpha_x \overline{v}_x + D_m$

Hydrodynamic Dispersion D_x caused by molecular diffusion and variations in the velocity field and heterogeneities

where:

$$\alpha_x$$
 = dispersivity [L]
 D_m = Molecular diffusion

$$F_{x} = v_{x}nC - nD_{x}\left(\frac{\partial C}{\partial x}\right)$$

• Flux = (mass/area/time)

(-) sign before dispersion term indicates that the contaminant moves toward lower concentrations

$$F_x = v_x nC - nD_x \left(\frac{\partial C}{\partial x}\right)$$

Total amount of solute entering the cubic element

$$= F_x dy dz + F_y dx dz + F_z dx dy$$

• Difference in amount entering and leaving element = $\mathcal{F} = \mathcal{F} = \mathcal{F}$

$$\left(\frac{\partial F_x}{\partial x} + \frac{\partial F_y}{\partial y} + \frac{\partial F_z}{\partial z}\right) dx dy dz$$

 For nonreactive solute, difference between flux in and out = amount accumulated within element

Rate of mass change in element =

$$n\left(\frac{\partial C}{\partial t}\right) dx dy dz$$

• Equate two equations and divide by dV = dxdydz: $(\partial F_{u}) (\partial F_{v}) (\partial F_{c}) (\partial C)$

$$-\left(\frac{\partial F_x}{\partial x}\right) + \left(\frac{\partial F_y}{\partial y}\right) + \left(\frac{\partial F_z}{\partial z}\right) = n\left(\frac{\partial C}{\partial t}\right)$$

Substitute for fluxes and cancel n:

 $-\left[\frac{\partial}{\partial x}(\bar{v}_{x}C)+\frac{\partial}{\partial y}(\bar{v}_{y}C)+\frac{\partial}{\partial z}(\bar{v}_{z}C)\right]+$

$$\left\{\frac{\partial}{\partial x}\left[D_{x}\left(\frac{\partial C}{\partial x}\right)\right] + \frac{\partial}{\partial y}\left[D_{y}\left(\frac{\partial C}{\partial y}\right)\right] + \frac{\partial}{\partial z}\left[D_{z}\left(\frac{\partial C}{\partial z}\right)\right]\right\} = \frac{\partial C}{\partial t}$$

 For a homogenous and isotropic medium, v is steady and uniform.

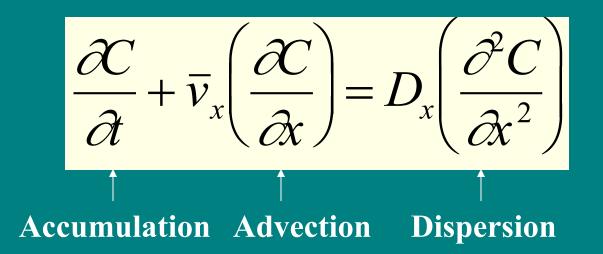
- For a homogenous and isotropic medium, is steady and uniform.
- Therefore, D_x , D_y , and D_z do not vary through space.

$$\left[D_x\left(\frac{\partial^2 C}{\partial x^2}\right) + D_y\left(\frac{\partial^2 C}{\partial y^2}\right) + Dz\left(\frac{\partial^2 C}{\partial z^2}\right)\right]$$

Advection-Dispersion Equation 3-D:

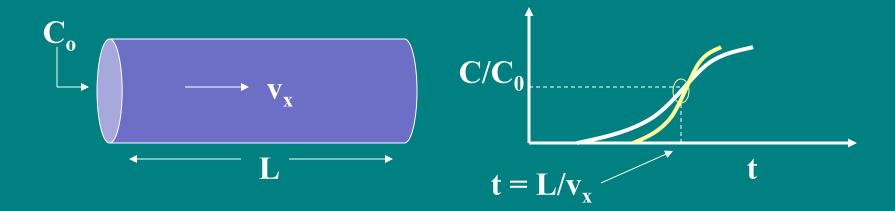
$$-\left[\overline{v}_{x}\left(\frac{\partial C}{\partial x}\right) + \overline{v}_{y}\left(\frac{\partial C}{\partial y}\right) + \overline{v}_{z}\left(\frac{\partial C}{\partial z}\right)\right] = \frac{\partial C}{\partial t}$$

In 1-D, the AD equation thus becomes:



CONTINUOUS SOURCE

 Solution for 1-D Equation for can be found using Laplace Transform



• 1-D soil column breakthrough curves

Solution can be written

 $\frac{C}{C_0} = \frac{1}{2} Erfc \left(\frac{L - v_x t}{\sqrt{4D_x t}} \right) + \left(\frac{1}{2} \right) Exp \left(\frac{v_x L}{D_x} \right) Erfc \left(\frac{L - v_x t}{\sqrt{4D_x t}} \right)$

or, in most cases

$$\frac{C}{C_0} = \frac{1}{2} Erfc \left(\frac{L - v_x t}{\sqrt{4D_x t}} \right)$$

where

$$Erfc(B) = 1 - Erf(B)$$
$$Erf(B) = \frac{2}{\sqrt{\pi}} \int_{0}^{B} e^{-z^{2}} dz$$

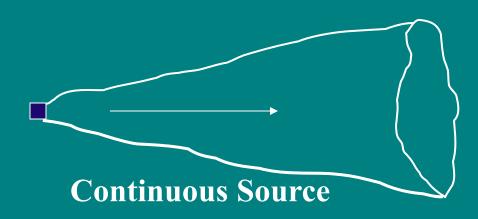
Tabulated error function

Instantaneous Sources Advection-Dispersion Only

Instantaneous POINT Source 3-D:

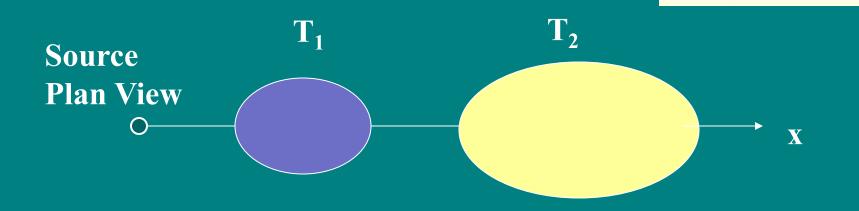
$$C(x,y,z,t) = \frac{M}{(4\pi Dt)^{3/2}} \exp\left(-\frac{(x-vt)^2}{4D_x t} - \frac{y^2}{4D_y t} - \frac{z^2}{4D_z t}\right)$$

 $M = C_0 V$ $D = (D_x D_y D_z)^{1/3}$



Instantaneous LINE Source 2-D Well: (with First Order Decay)

$$C(x,y,t) = \frac{m}{4\pi Dt} \exp\left(-\frac{(x-vt)^2}{4D_x t} - \frac{y^2}{4D_y t} - kt\right) \qquad \begin{array}{l} k = first \ order \\ decay \ (t^{-1}) \\ m = C_o A \\ D = \sqrt{D D} \end{array}$$



-x v

Instantaneous PLANE Source - 1 D

$$C(x,t) = \frac{M}{\sqrt{4\pi D_x t}} Exp\left(-\frac{(x-vt)^2}{4D_x t}\right) \qquad M = \frac{mass}{area}$$
AD Equation
$$\frac{\mathcal{X}}{\mathcal{A}} + \overline{v_x}\left(\frac{\mathcal{X}}{\mathcal{A}}\right) = D_x\left(\frac{\partial^2 C}{\partial x^2}\right)$$

$$C/C_0 \qquad t$$

$$T = L/v_x$$